

GUJARAT TECHNOLOGICAL UNIVERSITY**M. E. - SEMESTER – II • EXAMINATION – SUMMER • 2013****Subject code: 1723903****Date: 03-06-2013****Subject Name: Thermal Equipment Design****Time: 10.30 am – 01.00 pm****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Use of Steam table, Property table and Refrigeration table are permitted.

- Q.1 (a)** Discuss the effect of fouling on the performance of heat exchangers. **07**
- (b)** A surface condenser used in power plant have 10m long, 3cm in diameter 12 nos. of tubes. The flow rate of cooling water is 1.1 kg/s. The inlet and outlet temperature of cooling water are 25°C and 60°C respectively. Determine (i) mass flow rate (ii) overall Heat Transfer Co-efficient (iii) NTU (iv) Effectiveness. Take $h_{fg} = 2257 \text{ KJ/Kg}$ **07**

- Q.2 (a)** State the basic design procedure for heat exchanger. **04**
- (b)** A double pipe heat exchanger consists of tube of 40.09mm inner diameter and 48.3 mm outer diameter surrounded by a shell of 96.66mm bore. Dowtherm flowing in a tube at a rate of 2 kg/s is heated from 25°C to 55°C by hot water in counter flow in the annulus cooling from 90°C to 80°C. Calculate the length of the heat exchanger to achieve these temperatures. Use $Nu = 0.023 Re^{0.8} Pr^{0.4}$ **10**

OR

- (b)** A double pipe heat exchanger is employed to heat raw water ($m_c = 5 \text{ kg/s}$) from 15°C to 65°C using waste hot water ($m_h = 4.83 \text{ Kg/s}$) cooled in the process from 95°C to 75°C. The hot water flows in the inner tube (ID = 40mm, OD = 48mm) with 25 nos. of longitudinal carbon steel fins (Fin Width = 0.89mm, Fin Height = 12mm & Root Width = 4mm) in counter flow to the raw water which flows in annulus (ID = 75mm, OD = 89mm). Calculate the length of the tubes. Consider $K_{fin \text{ material}} = 60 \text{ W/m}^0\text{K}$. Use $Nu = 0.023 Re^{0.8} Pr^{0.4}$ **10**

- Q.3 (a)** Write a short note on shell and coil type evaporator. **07**
- (b)** The following are the values measured on a shell-and-tube ammonia condenser: **07**

Velocity of water flowing through the tubes, V m/s	1.25	0.63
Overall heat transfer co-efficient, $U_0 \text{ W/m}^2\text{K}$	2250	1540

Water flowed inside the tubes while refrigerant condensed outside the tubes (OD-45mm, ID-40mm, $K = 60 \text{ W/mK}$). Using the concept of Wilson's plot, determine the condensing heat transfer coefficient. What is the value of overall heat transfer coefficient when the velocity of water is 0.22 m/s?

OR

- Q.3 (a)** Give a note on tube in tube type condenser. **04**

- (b) Distilled water with flow rate of 50 kg/s enters a baffled shell & tube heat exchanger at 32°C and leaves at 25°C. Heat will be transferred to 150 kg/s of raw water coming from a supply at 20°C and leaving at 22.33°C. Using Bell Delaware method, calculate the shell diameter of heat exchanger for the following data: tube O.D.: 19mm, tube I.D.: 16mm, Square tube pitch: 25.4mm, baffle spacing: 0.5m (25% cut), max. Length = 8m, $K_{\text{tube}} = 42.3 \text{ W/m} \cdot \text{K}$, Total fouling resistance = 0.000176 m².K/W. Surface over design should not exceed 30%. The max. flow velocity through the tube is 2 m/s. Assume combined effect of correction factors = 60%. Nusselt no. for hot fluid is 132 and for cold fluid is 224. $j_i = 0.0081$. No. of tubes = 350. CL = 1, CTP = 0.93 PR = 1.33. 10

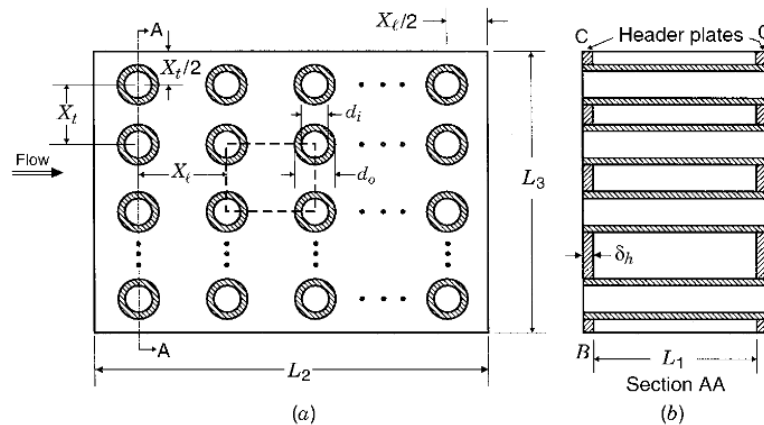
Q.4 (a) Explain the step by step calculation procedure for a rating problem in a compact heat exchanger. 07

- (b) Air at 2 atm and 500 K with a velocity of 20 m/s flows across a compact heat exchanger matrix having the configuration shown in Figure-1 (surface 11.32-0737-S-R). Calculate the heat transfer coefficient and the frictional pressure drop. The length of the matrix is 0.8 m. 07

OR

Q.4 (a) Explain factors influencing tube-fin heat exchanger performance in compact heat exchanger. 07

- (b) Find out different geometrical characteristics of tubular heat exchanger as shown in figure, where $L_1=200\text{mm}$, $L_2=300\text{mm}$, $L_3=300\text{ mm}$, $d_i=10.67\text{mm}$, $d_o= 21.87 \text{ mm}$, $\delta_h=2.9134 \text{ mm}$ 07



Q.5 (a) Explain different components of induced draft cooling tower. 07

- (b) The findings of one typical trial pertaining to the Cooling Towers of a Thermal Power Plant 3 x 200 MW is given below: 07

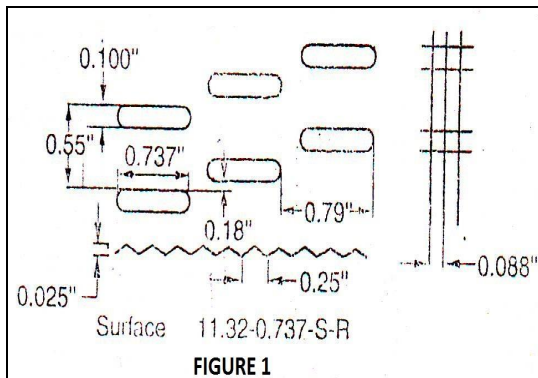
- * Unit Load 1 & 3 of the Station = 398 MW
- * Mains Frequency = 49.3
- * Inlet Cooling Water Temperature °C = 44 (Rated 43°C)
- * Outlet Cooling Water Temperature °C = 37.6 (Rated 33°C)
- * Air Wet Bulb Temperature near Cell °C = 29.3 (Rated 27.5°C)
- * Air Dry Bulb Temperature near Cell °C = 40.8°C
- * Number of CT Cells on line with water flow = 45 (Total 48)
- * Total Measured Cooling Water Flow m³/hr = 70426.76
- * Measured CT Fan Flow m³/hr = 989544

Analyze the cooling tower and comment on the results obtained in the analysis

OR

Q.5 (a) Explain the factors affecting the cooling tower performance. 07

- (b) A chiller plant system (capacity 500kW) with COP at 4.5 is designed with a cooling tower, the design entering and leaving condenser water temperature of the cooling tower are 37°C and 32°C respectively, the design wet bulb temperature of the outdoor air is 28°C, what are: 07
- the cooling tower coefficient
 - the required condenser water and air mass rate (in kg/s) in the cooling tower
 - the required height of the fill



Properties of Air at 2 atm pressure

Temperature [Celsius]	200	250
Density : [kg / m ³]	1.49	1.36
Specific Enthalpy : [kJ / kg]	475.95	527.76
Specific Entropy : [kJ / kg K]	7.22	7.31
Specific isobar heat capacity(c_p) [kJ / kg K]	1.03	1.04
Heat conductance [10 ⁻³ W/m*K]	37.98	41.05
Dynamic viscosity : [10 ⁻⁶ (Pa s)]	26.10	27.98
Kinematic viscosity : [10 ⁻⁶ m ² / s]	28.20	33.64
Thermal diffusivity : [10 ⁻⁷ m ² / s]	399.86	475.89
Prandtl-Number :	0.71	0.71

